THE OPTIMIZATION AND MATHEMATICAL MODELS DETERMINATION OF COPPER RECOVERY – THE PRECONDITION FOR IMPROVEMENT OF RECOVERY IN BUCIM COPPER MINE

A. Krstev, B. Krstev, Z. Zdravev, Zivko Gocev, J. Zivanovic, D. Krstev

¹University "Goce Delchev", Faculty of Natural and Technical Sciences, Shtip, R. of Macedonia

ABSTRACT. The improvement in the chalcopyrite copper Bucim mine are gone forward to renewed reagent regime, including and involving new reagents for increase d recovery of copper and gold. The optimization and mathematical linear models using gradient method Box and Wilson are good example for improvement of industrial recoveries in flotation circuit. In this paper is shown optimization techniques, formatting the mathematical model and adequate model for carried out investigations. Tables and figures will show the optimal quantity in reagent regime (collectors), particle size, flotation time I rougher flotation, conditioning time etc.

KEYWORDS: investigation, mathematical, model, recovery, flotation, Bucim

INTRODUCTION

The previous carried out laboratory investigations with application of the new collectors CYTEC and frothers confirmed that there is possibility for significantly improvement of the gold recovery with same copper quality and decreasing of the CaO consumption. The investigations with reagents Aerophine 3404, Aero XD 5002 and frother OP-F49 in the previous period (2010) were very short because of the low quality and variations of the ores. Variations of the ore from 0.15-0.22%Cu, instability of the flotation and other problems in the flotation process. The combination of the Aerophine 3404, KEX:KBX= 1:1, NaIPX, SKIK Bz 2000, in the different points of the flotation process gave significantly better results that early. The process was prolonged with pH=10.5 and the point of addition of CaO was at the hydro cyclone (70%) and 30% in the flotation process. The conclusions of these investigations were very heavy for sure confirmation, bur the obtained results were close to the previous results by standard conditions (specially for Au), may be better but not significantly. The Au content in the ore was од 0,19-0,29 gr/t, in the concentrate 8-12,3 gr/t, with Au recovery from 45-55% (some appearances up to 60%), but the copper recovery in the standard interval. Considering these investigations in laboratory and industrial real conditions may be concluded that:

- The instability and relative short period of investigations in the real conditions have contributed for obtaining the technological parameters closed to the standard conditions.
- As a result of the good regrinding, it was very heavy to clean the rough concentrate Cu/Au,
- Using higher pH, higher than standard in the rougher flotation (elimination of pyrite flotation) by Aerophine 3404, it will be expected higher quality and content of Cu/Au,
- In the existing real conditions of flotation at pH 11,0-11,6 and consumption of Aerophine 3404 (AP3404) from 18-22 гρ/τ, together with change of adaptive changeable reagent regime by different collectors (the combination from Aerophine 3404, KEX:KBX, NaIPX),
- The prolonged changes of the reagent regime with contemporary addition of new reagents (Bz 2000 = 4-8 gr/t + KEX:KBX=1:1 = 8-4 gr/t, total 12 gr/t) in the grinding cycle, together with addition of NaIPX in the condictioner with 8-10 gr/t, in the flotation process (rougher and controlled flotation) with 2-4 gr/t, or total addition of 14 gr/t NaIPX,

Full Factorial Plan of experiments for three factors in Bucim mine

The plan of experiments is carried out for existing regent regime in the flotation plant in Bucim mine. The obtained result are given in the following table 1 and table 2:

Tabl. 1 Tests with a plan experiments

Опит	X _o	X ₁	X ₂	X ₃	I ₁	I ₂	I _{Cu} % _{sr}
1	+	15	10	5	90,13	89,05	89.59
2	+	15	6	5	90,52	87,90	89.21
3	+	9	10	5	89,18	88,80	88.99
4	+	9	6	5	86,66	87,22	86.94
5	+	15	10	3	89,10	87,22	88.16
6	+	15	6	3	88,60	90,48	89.54
7	+	9	10	3	88,90	89,62	89.26
8	+	9	6	3	88,00	87,08	87.54

Tabl. 2 Tests with a plan experiments

Опит	Xo	X ₁	X ₂	X ₃	I_1	I ₂	Ic.//h.s	Losso	ΔI
1	+	15	10	5	90,13	89,05	89,59	88,87	0,72
2	+	15	6	5	90,52	87,90	89.21	87,93	1,28
3	+	9	10	5	89,18	88,80	88.99	88,18	0,81
4	+	9	6	5	86,66	87,22	86.94	87,24	0,30
5	+	15	10	3	89,10	87,22	88.16	90,06	1,90
6	+	15	6	3	88,60	90,48	89.54	89,12	0,42
7	+	9	10	3	88,90	89,62	89.26	89,37	0,11
8	+	9	6	3	88,00	87,08	87.54	88,43	0,89

Considering the obtained results will be carried out analysis of the obtained linear model, establishing his adequate. As the model is obtained on the basis of the mean values of recoveries, then the productivity error for the mean values will be:

$$\bar{S}_{rtsr}^2 = \underbrace{\begin{bmatrix} (9013 - 8905)^2 + (9052 - 8790)^2 + (8918 - 8880)^2 + (8666 - 8722)^2 \\ + (8910 - 8722)^2 + (8860 - 9048)^2 + (8890 - 8962)^2 + (8800 - 8708)^2 \end{bmatrix} }_{4}$$

$$\overline{S}_{rlsr.}^2 = 0,264; \ \overline{S}_{rlsr.} = \sqrt{0,264} = 0,514$$

²Mine BUCIM, Radovis, R. of Macedonia

³University "Goce Delchev", Faculty of Computer Science, Shtip, R. of Macedonia

Adequate model checking

After the estimation of the investigated model, it's needed to calculate the mean result of each test, and instead x_j in the mentioned model we'll put appropriate conditioned units of the test (± 1) :

$$I_{pres.1} = 88,65 + 0,346 (+1) + 0,47 (+1) - 0,596 (+1) = 88,87$$

$$I_{pres,2} = 88,65 + 0,346 (+1) + 0,47 (-1) - 0,596 (+1) = 87,93$$

$$I_{pres.3} = 88,65 + 0,346 (-1) + 0,47 (+1) - 0,596 (+1) = 88,18$$

$$I_{pres.4} = 88,65 + 0,346 (-1) + 0,47 (-1) - 0,596 (+1) = 87,24$$

$$I_{pres.5} = 88,65 + 0,346 (+1) + 0,47 (+1) - 0,596 (-1) = 90,06$$

$$I_{\text{pres},6} = 88,65 + 0,346 (+1) + 0,47 (-1) - 0,596 (-1) = 89,12$$

$$I_{pres.7} = 88,65 + 0,346 (-1) + 0,47 (+1) - 0,596 (-1) = 89,37$$

$$I_{pres.8} = 88,65 + 0,346 (-1) + 0,47 (-1) - 0,596 (-1) = 88,43$$

In the above table are given errors $\Delta I = I_{\text{sr.}} - I_{\text{pres.}}$, and the model adequate may be checked by Fischer criteria:

$$F = \frac{\left[\sum_{i=1}^{N} I_{sr.i}^{2} - N \cdot \sum_{i=0}^{k} b_{i}^{2}\right]}{(N - k - 1) \cdot S_{rlsr.}}$$

Where: k- number of linear members in the mentioned model. In our case we'll have:

$$\begin{array}{l} F = [89,59^2 + 89,21^2 + 88,99^2 + 86,94^2 + 88,16^2 + 89,54^2 + 89,26^2 \\ + 87,54^2] - 8[88,65^2 + (0,346)^2 + 0,47^2 + (0,03)^2 + (-0,596)^2 + 0,26^2 \\ + 0,24^2 + 0,18^2] \ / \ 5 * 0,514 \ ; \end{array}$$

For $f_b=8-2-1=5$ and $f_r=8(2-1)=8$, for confidential level p=95%=3,69, and Student = 2,306, Fischer criteria:

$$F^* = f_r + p + t = 8 + 3,69 + 2,306 = 13,996.$$

As $F \ll F^*$, the model is adequate. It means that investigated process is correct described by means of the first order pollinom and the difference which is appeared between experimented and estimated results is accidental

The determination of the obtained linear model gradient for reagent regime in the flotation plant in Bucim mine

The gradient method is based on the fact that biggest degree of improvement for a function is achieved if the progressive by the length of the gradient. As this direction is direction of the steeper gradient, then we're talking about for maximum, or the direction of the steeper fall. In fact, the gradient is vector for a point of the n-dimensional space. This one is determined by the determination of the first derivations of the aim function in the relationship of their changeable factors. It's important to note that the gradient direction is a local, not a global property. If we suppose that the function $\gamma(x_1, x_2)$, which has had continuous partial derivations, then there is the point (x_1, x_2) , around which for a little small change in the every one direction will be obtained the following estimation.

$$\frac{df}{dx_1}(x_1, x_2) = \frac{df(88.65 + 0.346 x_1 + 0.47 x_2 - 0.596 x_1 x_2)}{dx_1} = -4,422$$

$$\frac{df}{dx_2}(x_1, x_2) = \frac{df(88.65 + 0.346 x_1 + 0.47 x_2 - 0.596 x_1 x_2)}{dx_2} = -6,682$$

$$m_1 = \frac{\frac{df}{dx_1}(x_1)}{\sqrt{(\frac{df(x)}{dx_1})^2 + (\frac{df(x)}{dx_2})^2}} = \frac{-4,422}{8,012} = -0.55$$

$$m_2 = \frac{\frac{df}{dx_1}(x_2)}{\sqrt{(\frac{df(x)}{dx_1})^2 + (\frac{df(x)}{dx_2})^2}} = \frac{-6,682}{8,012} = -0,83$$

The moving direction will be shown as a vector ϕ marked with n numbers $(m_1, m_2 \dots m_n)$.

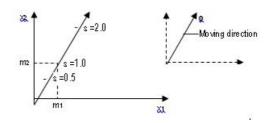


Fig. 1. Direction of search

$$\frac{m_1}{m_2} = \frac{-0.55}{-0.83} = 0.663$$

$$m_1 \cdot \Delta x_1 = -0.55 \cdot 3 = -1.65$$

$$m_2 \cdot \Delta x_2 = -0.83 \cdot 2 = -1.66$$

It's evident that gradient direction is exact, and x_1 and x_2 has had to be adjuste, because the coefficient of interaction b_{12} with his sign show this action. Standard deviation $\sigma = \sqrt{\frac{\sum \Delta f^2}{7}} = 1.03$.

By the analysis of the linear model of the first order polinom for copper recovery from the chalcopyrite ore, above mentioned equations for carried out investigations by decreasing of the collector $(x_1-NaIPX)$ and with increasing of the $(x_2-KEX:KBX=1:1)$, we'll be obtained following results in table 4.

Tabl. 3 Tests with a plan experiments

Tie		CS WICH U					
	I ₁	I ₂	I _{Cu} % _{sr}	\mathbf{I}_{pres}	ΔΙ	ΔΙ	² ΔΙ ² /7
	90,13	89,05	89.59	88,87	0,72	0,52	
	90,52	87,90	89.21	87,93	1,28	1,64	
	89,18	88,80	88.99	88,18	0,81	0,65	
ľ	86,66	87,22	86.94	87,24	-0,30	0,09	1,07
	89,10	87,22	88.16	90,06	-1,90	3,61	
	88,60	90,48	89.54	89,12	0,42	0,17	
ľ	88,90	89,62	89.26	89,37	-0,11	0,01	
Ĺ	88,00	87,08	87,54	88,43	-0,89	0,79	

Tabl.4 Tests with a plan experiments

ests with a plan experiments								
Опит	X ₁	X ₂	I ₁	\mathbf{I}_2	$I_{\text{Cu}}\%_{\text{sr}}$			
1	11.5	10.5	90.0	89.2	89.6			
2	11.5	9.5	90.4	90.0	90.2			
3	9.5	10.5	90.1	89.3	89.7			
4	9.5	9.5	89.7	89.3	89.5			
5	11.5	10.5	89.2	89.2	89.2			
6	11.5	9.5	89.2	90.0	89.6			
7	10	10.5	90.4	90.2	90.2			
8	9.5	9.5	88.7	88.3	88.5			

The other working parameters (pH=11.72, $55 \div 60\%$ - 0,074 mm, flotation time 12 min and time of conditioning 6 min and $X_3 = 4 \div 6$ gr/t) are standard as in the real industrial conditions. The copper recovery in the $I_{\text{Cu}}\%_{\text{sr}}$ is optimal or need minimum decreasing of collector consumption of NaIPX = 10-11.5, and increasing of KBX:KEX=1:1 = $9.5 \div 10.5$ gr/t, according to the influence of the feed ore quality, bigger content of copper in the feed, bigger consumption of the collectors.

CONCLUSION

In this paper is shown optimization techniques with formatting the mathematical model and adequate model for carried out investigations. Obtained tabular results and figures will show the optimal quantity in reagent regime (collectors), particle size, flotation time for rougher flotation, conditioning time etc.

REFERENCES

- Mular, A. L., (1980). "Empirical modeling and aptinusation of mineral
- Mular, A. L., (1980). "Empirical modeling and aptinusation of mineral processes", Mineral Science and Engineering, 4, No 3. Pp 30-42.
 Napier-Munn, T. J., Morrell, S., Morrison, R. D., and Kojovic, T., (1996). "Mineral comminution circuits: their operation and optimization". JKMRC., pp. 413.
 Plitt, L. R., (December, 1976). "A mathematical model of the hydrocyclone classifier", CIM Bull. 69, 114.
 Povarov A. I., (1978). "Gridrocikloninaobogatitel'nyhfabrikah", "Nedrya Pussia.
- Povarov A. I., (1978). "Nedra". Moskva, Russia.
- Renner, V. G., and Cohen, H. E., (June, 1978). "Measurement and
- interpretation of size distribution of particles within a hydrocyclone", *Trans. IMM.*, Sec. C, 87,139.

 Rowland C. A., (1986). "Ball Mill Scale-up-Diameter Factors., Advances in Mineral Processing", P. Somasundaran Editor Society of Mining Engineers (ATME 24, 605).
- of Mining Engineers/AIME, 34, 605. Svarovsky, L., (1984). "Hydrocyclones", Holt, Rinehart & Winston Ltd, Eastbourne.
- Wiegel R. L., and Li K. A., (1986). "Random Model for Mineral Liberation by Size Reduction", Trans. AIME, 238, 179.
 Wills, B. A. (1988). "Mineral Processing Technology", 4th edition