

# Determination of Possibility of the Segregation Process Intensification Nickel from Ni-ores by Goles Locality,

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## Abstract

The same is the interest and perspective of the segregation process. The previous investigations in the field of the metal compounds chlorination, especially the chlorination of the refractory nickel minerals: garnierite and nontronite, by the chlorine, HCl or NaCl or CaCl<sub>2</sub>, were determined directions, confirming the perspective of the mentioned process for the treatment of the low grade and complex minerals-laterites.

## 1. Introduction

The principal scheme of the segregation process following by the classical concentration methods - flotation or magnetic separation and hydrometallurgical treatment - ammonia leaching is shown on the figure 1. The combined methods for enriching of the oxide-silicate nickel ores are these through which by heating the ore with coke and CaCl<sub>2</sub> at high temperature metal nickel is formed on the present coke, or on the silicates which are the component parts of the ore.

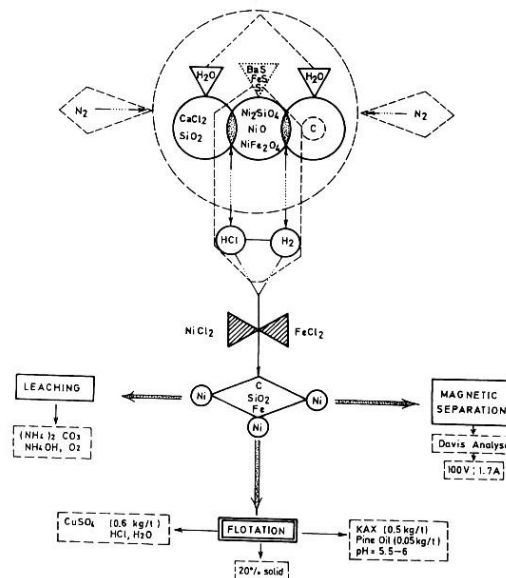
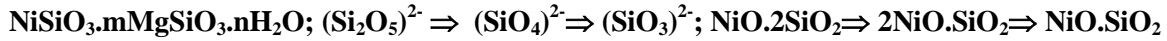


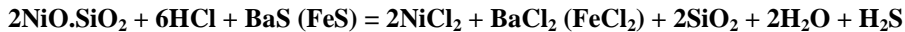
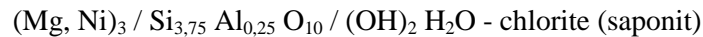
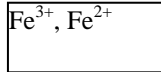
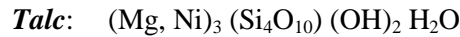
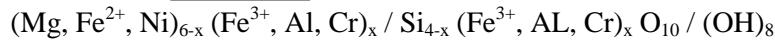
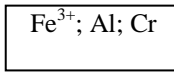
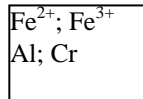
Fig. 1 Principal scheme of segregation process

## 2. The general behaviour of the nickel bearing minerals

For the metallurgical calculation Ni in the oxide-silicated minerals may be shown by means of the general formula:



The iron in these Ni - bearing minerals and ores is appeared as  $\text{Fe}_2\text{O}_3 \cdot n\text{H}_2\text{O}$  and as a nontronite  $(\text{Fe,Al})_2(\text{Si}_4\text{O}_{10})(\text{OH})_2 \cdot n\text{H}_2\text{O}$ . The oxide-laterite ores are with low nickel content. The generally, nickel and iron are as **Ni-Fe-limonite**  $(\text{Fe,Ni})\text{O}(\text{OH}) \cdot n\text{H}_2\text{O}$  or in the talc form,  $(\text{Mg, Ni})_3(\text{Si}_4\text{O}_{10})(\text{OH})_2 \cdot \text{H}_2\text{O}$ .



The thermodynamic characteristic of the above mentioned reactions are performed using the standard isobaric potential and for working on the kinetic characteristic of the chlorination - segregation process have used the equations which describe the reaction controlled by three-dimensional surfaces advancement (diffusion-controlled reactions and reaction-controlled reactions).

### 3. The experimental investigations from the nickel bearing ore Goles by segregation process

The segregation process of the nickel bearing ore Goles and chlorination addition  $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$ , reduction coke is conducted at the temperature (1023-1223°K) with retaining time (20-120 min) in the atmosphere of  $\text{N}_2$ . The experimental investigations by the addition-activator 2% ( $\text{BaS}$ ,  $\text{FeS}$ ,  $\text{S}$  or  $\text{BaSO}_4$ ) influence on the metallurgical indicators from combined processes **segregation-flotation-magnetic separation-ammonia leaching** are shown about the ore samples from various ore samples.

Table 1. Result obtained from segregation - flotation - magnetic separation - ammonia leaching

ORE GOLES	T (°C)	t (min)	Flotation	Magnetic sep.	Leaching
			$R_{\text{Ni}}$ (%)	$R_{\text{Ni}}$ (%)	$R_{\text{Ni}}$ (%)
1,25%Ni	750	20	1.62	1.50	1.70
		40	3.41	3.05	3.65
I Goles + 2% BaS	850	60	3.89	3.20	4.10
		20	8.43	7.80	8.70
		40	17.66	16.50	18.25
		60	25.43	21.25	27.10
	950	120	45.40	42.30	46.50
		20	28.32	25.10	30.05
		40	40.78	37.20	42.45
		60	44.78	40.00	5.75
		120	60.98	56.70	65.10
II Goles + 2% BaS	750	20	1.90	1.70	2.15
		40	3.82	3.25	4.20
		60	5.48	4.85	6.10
	850	20	14.36	12.10	16.10
		40	25.17	22.10	27.10
		60	37.40	33.45	40.00
		120	55.60	51.50	56.50
		20	36.85	32.40	39.60
		40	47.24	43.70	50.00
	950	60	58.73	55.10	64.05
		120	76.35	71.35	78.40
III Goles mix + 2% BaS	750	20	2.18	1.70	2.55
		40	3.82	3.25	4.20
		60	6.84	5.25	7.65
	850	20	17.55	16.50	18.25
		40	28.40	25.05	30.00
		60	44.65	40.00	46.00
		120	58.60	55.00	61.30
		20	33.42	30.15	35.10
		40	50.41	44.10	52.05
	950	60	59.25	56.00	65.00
		120	80.70	76.40	82.10

The partial chemistry composition from the ore samples (100% - 0,150mm and 100% - 0,100mm) are from 1,25%Ni, 1,37%Ni Goles I (both in Kosovo-Yugoslavia ), 1,2%Ni and 1,86%Ni Goles II (both in Kosovo-Yugoslavia).

#### 4. The experimental investigations from the nickel natural ores by segregation process

The experimental investigations by the addition-activator 2% (BaS,FeS,S or BaSO<sub>4</sub>) influence on the metallurgical indicators from combined processes **segregation-flotation-magnetic separation-ammonia leaching** are shown about the ore samples from various deposits. The partial chemistry composition from the ore samples (100% - 0,150mm and 100% - 0,100mm) are from 0,85%Ni Studena voda, 0,97%Ni Rzanovo (both in Macedonia), 1,2%Ni and 1,86%Ni Rudjinci I & II (both in Yugoslavia).

Table 3. Results obtained from segregation - flotation of the ore samples (100% -0.150mm)

Ore sample	BaS (%)	Recovery (%), R <sub>Ni</sub>		
		Flotation	Magnetic separat.	Leaching
Goles I	0.0	46.50	54.70	60.20
	2.0	55.45	60.85	66.10
	3.5	63.70	65.60	69.35
Goles II	0.0	56.85	55.30	57.60
	2.0	70.10	66.60	68.20
	3.5	82.30	80.70	85.10
Goles I	0.0	62.50	60.25	63.10
	2.0	78.60	75.30	80.20
	3.5	85.00	83.20	86.75
Goles II	0,0	65,00	70,00	68,00
	2,0	78,50	80,50	82,30
	3,5	88,00	89,50	90,50

#### 5. Conclusion

The combined processes **segregation-flotation-magnetic separation ammonia leaching** by the synthetic mixures and appropriate ore samples (various nickel content) have achieved satisfactory results related on the metal recoveries. The existing environmental problems will lead to increased interest in combined processes or hydrometallurgical processes. These include combined processes: **segregation-flotation-ammonia leaching** or some other process as an oxidation and bio oxidation.

## 6. References

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